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Results of CLEVASOL Sorbent Testing at FSUE Mayak PA

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Test object: liquid high-level waste



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Monitored parameter	Unit	Value
Cs-137	Bq/L	$(2-5) \cdot 10^{10}$
Cs-134		$(2-3) \cdot 10^8$
$\Sigma\alpha$		$(1-100) \cdot 10^4$
$\Sigma\beta$		$(2-6) \cdot 10^{10}$
Total dissolved solids		400-450
Al	g/L	4.3
Na		162
Fe		0.3
Cr (CrO4)		2
Ca		3
Mg		0.8
Si		0.4
NO ₃ ⁻		161





CLEVASOL sorbent description



Full capacity (min.): 5,4 meq/g (H+ form)

Humidity: 45-55% (H+ form)

Grain Size: 200 ± 100 μm

Iron Impurity (max): 50 ppm

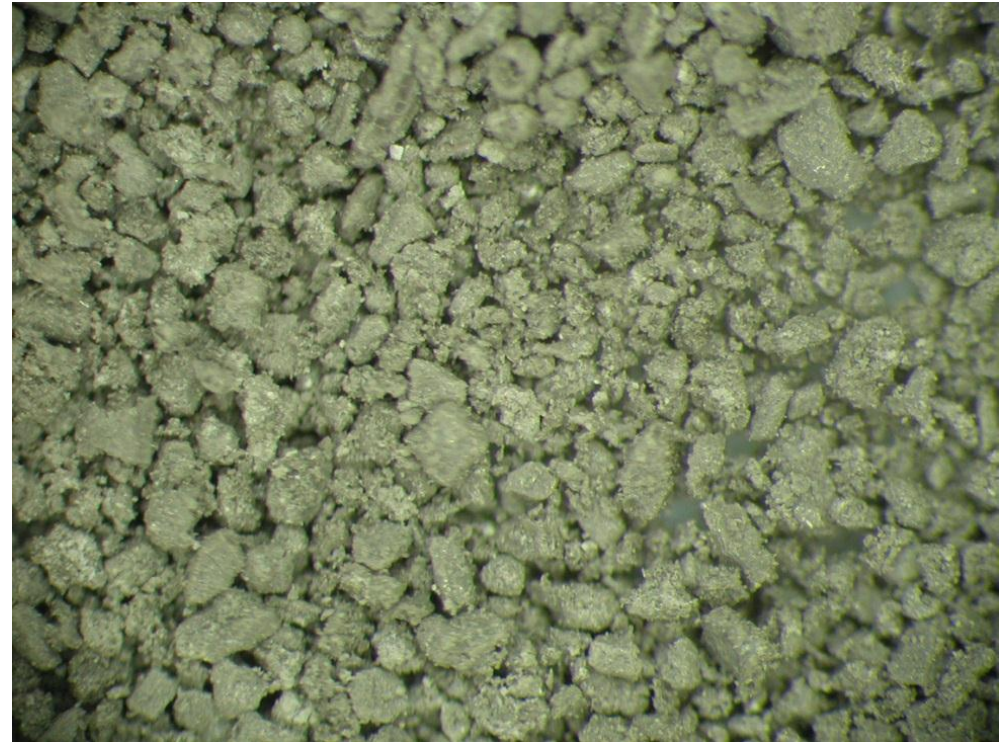
Sodium Impurity (max): 40 ppm

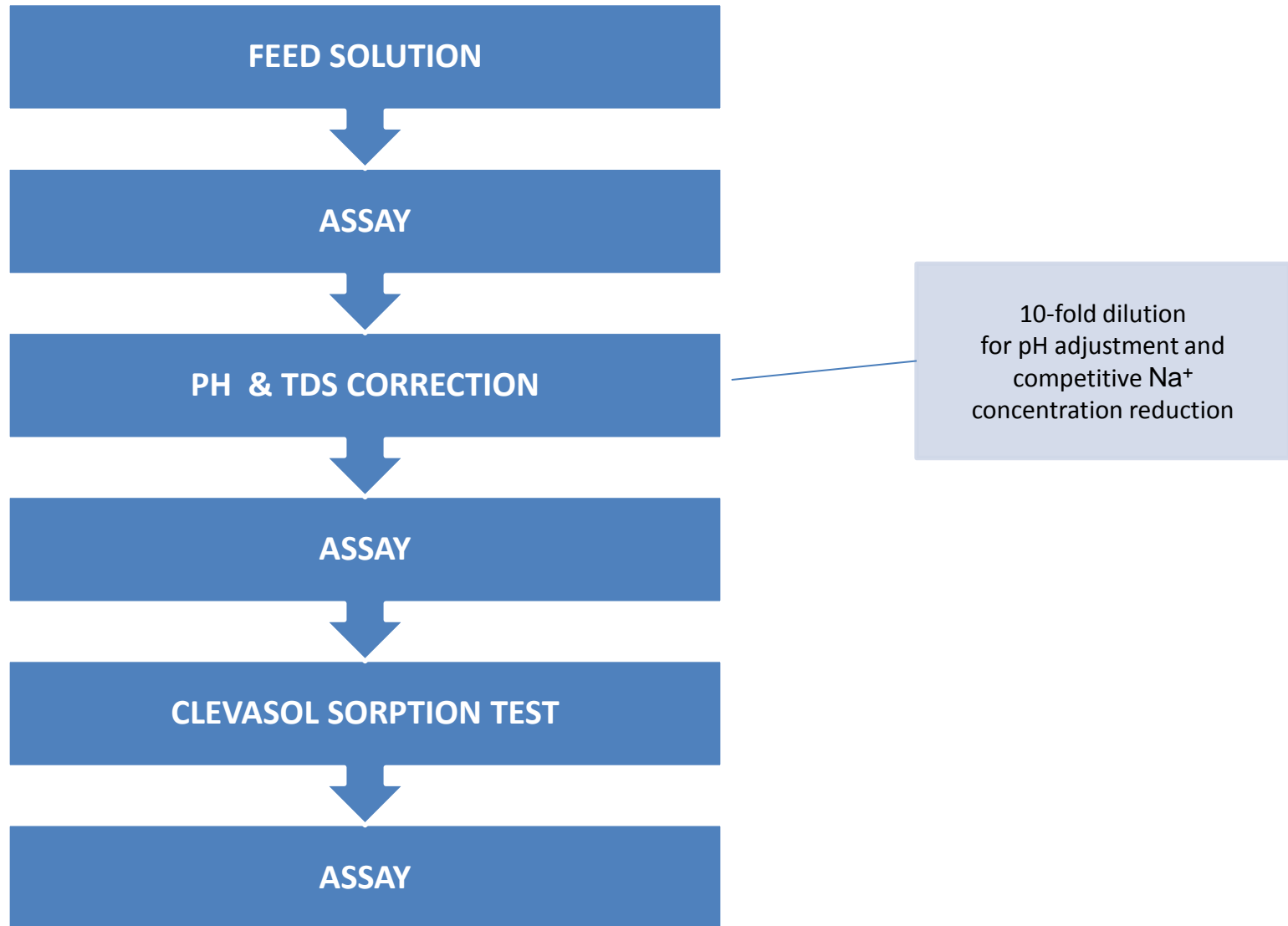
Heavy Metall Impurity (max): 40 ppm

Maximum Temperature: 160 °C

Density (approx.) (H+ form): 550 g/L

**Insoluble in water, acids, alkalis in pH range
from 0 to 14 and organic solvent**







CLEVASOL static sorption test with simulated solution



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Simulated solution

Waste Component	Concentration, mg/L			
	pH=12		pH=9	
	Feed Solution	Filtrate	Feed Solution	Filtrate
Na	9,900	3,064	8,650	5,310
Cs	5	0.281	1.9	<0.3

Solids : liquid = 1:10 Decontamination factors (DF) derived: 18 (94.4 %) for Cs

Active solution

Waste Component	Specific activity, Bq/L			
	pH=12		pH=9	
	Feed Solution	Filtrate	Feed Solution	Filtrate
Cs-137	$4.2 \cdot 10^9$	$2.0 \cdot 10^8$	$4.2 \cdot 10^9$	$1.7 \cdot 10^9$
$\Sigma\beta$	$3.4 \cdot 10^9$	$9.4 \cdot 10^7$	$3.4 \cdot 10^9$	$1.7 \cdot 10^8$

Solids : liquid = 1:10

Decontamination factors (DF) derived: 21 (95.2 %) for ¹³⁷Cs
36 (97.2 %) for $\Sigma\beta$

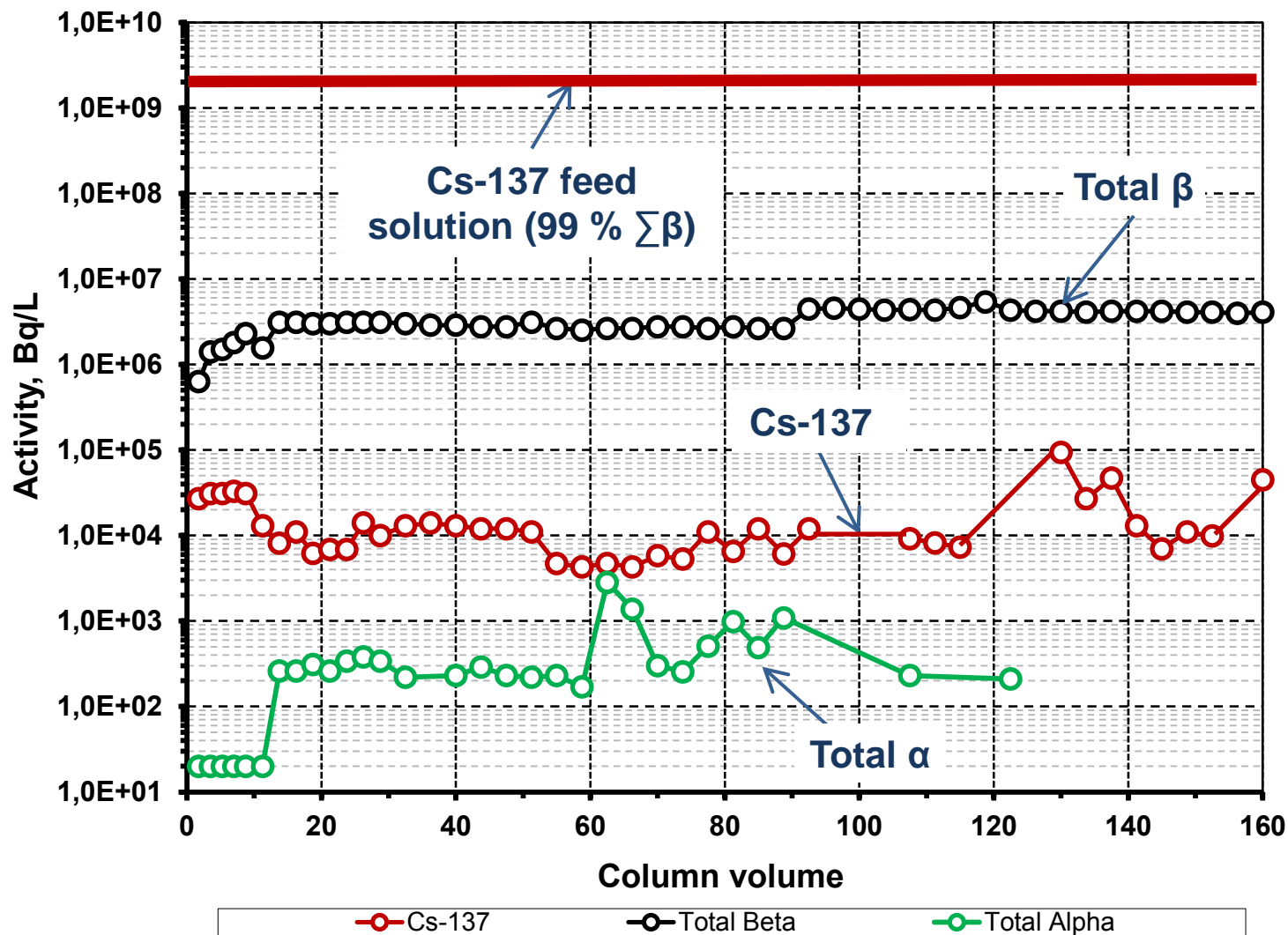




CLEVASOL dynamic sorption test with HLW solution (test 1)



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Feed solution
 $1.7 \cdot 10^9$ Bq/L ^{137}Cs
 $1.2 \cdot 10^7$ Bq/L ^{134}Cs
 $6.0 \cdot 10^6$ Bq/L ^{125}Sb
 $2.6 \cdot 10^6$ Bq/L ^{106}Ru
pH ~ 10.0

Averaged test results:

~ $7.4 \cdot 10^4$ Bq/L ^{137}Cs ,
DF = 23,000 (99.996 %)

~ 4,500 Bq/L ^{134}Cs ,
DF = 2,700 (99.96%)

$5.4 \cdot 10^5$ Bq/L ^{125}Sb ,
DF ~ 11 (91 %)

practically no
decontamination in
terms of ^{106}Ru , ^{144}Ce

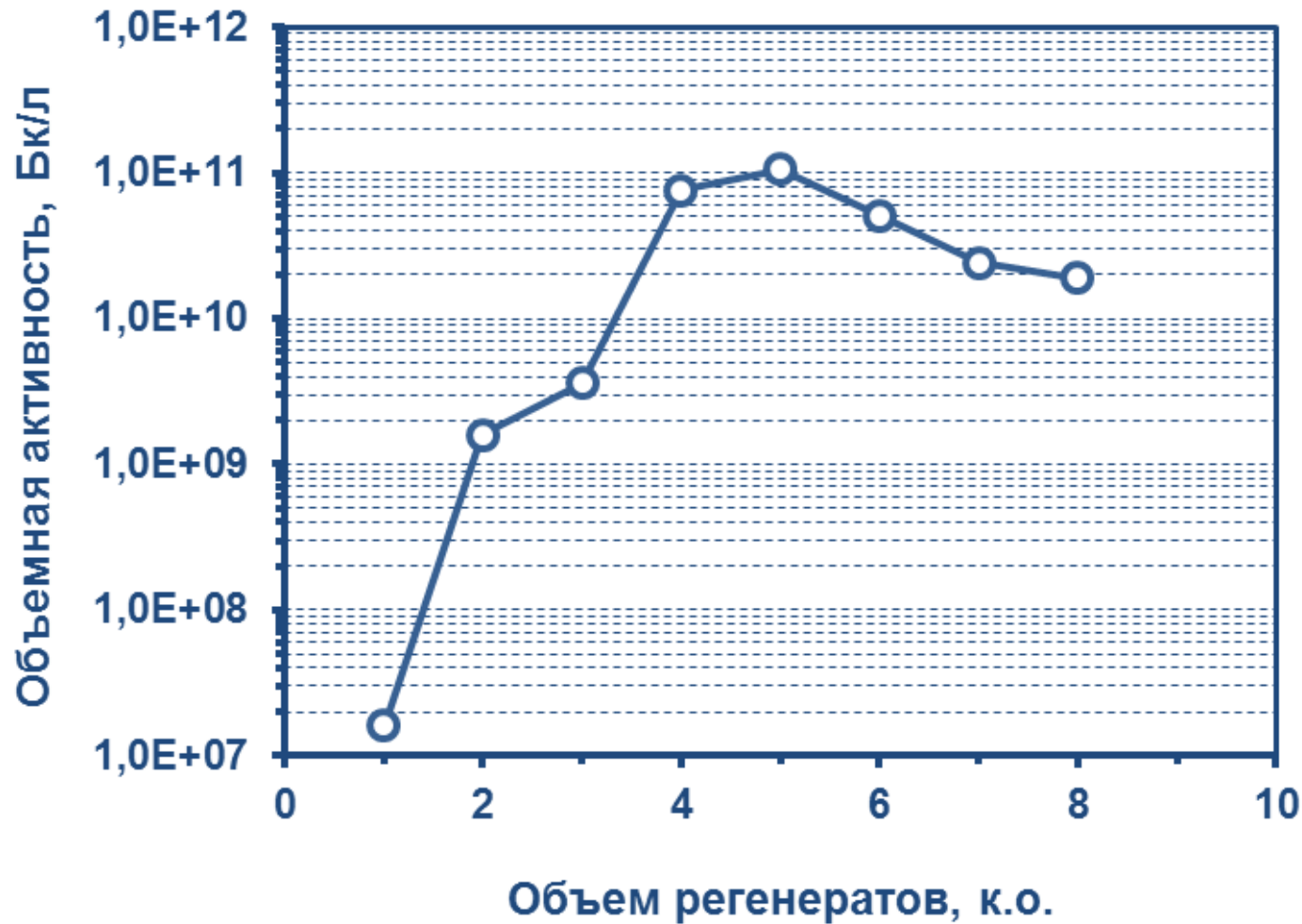




CLEVASOL regeneration (test 1)



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98% Cs-137 were removed with wash-off solution

Filter MED decreased from 600 μ R/s to 10 μ R/s after regeneration

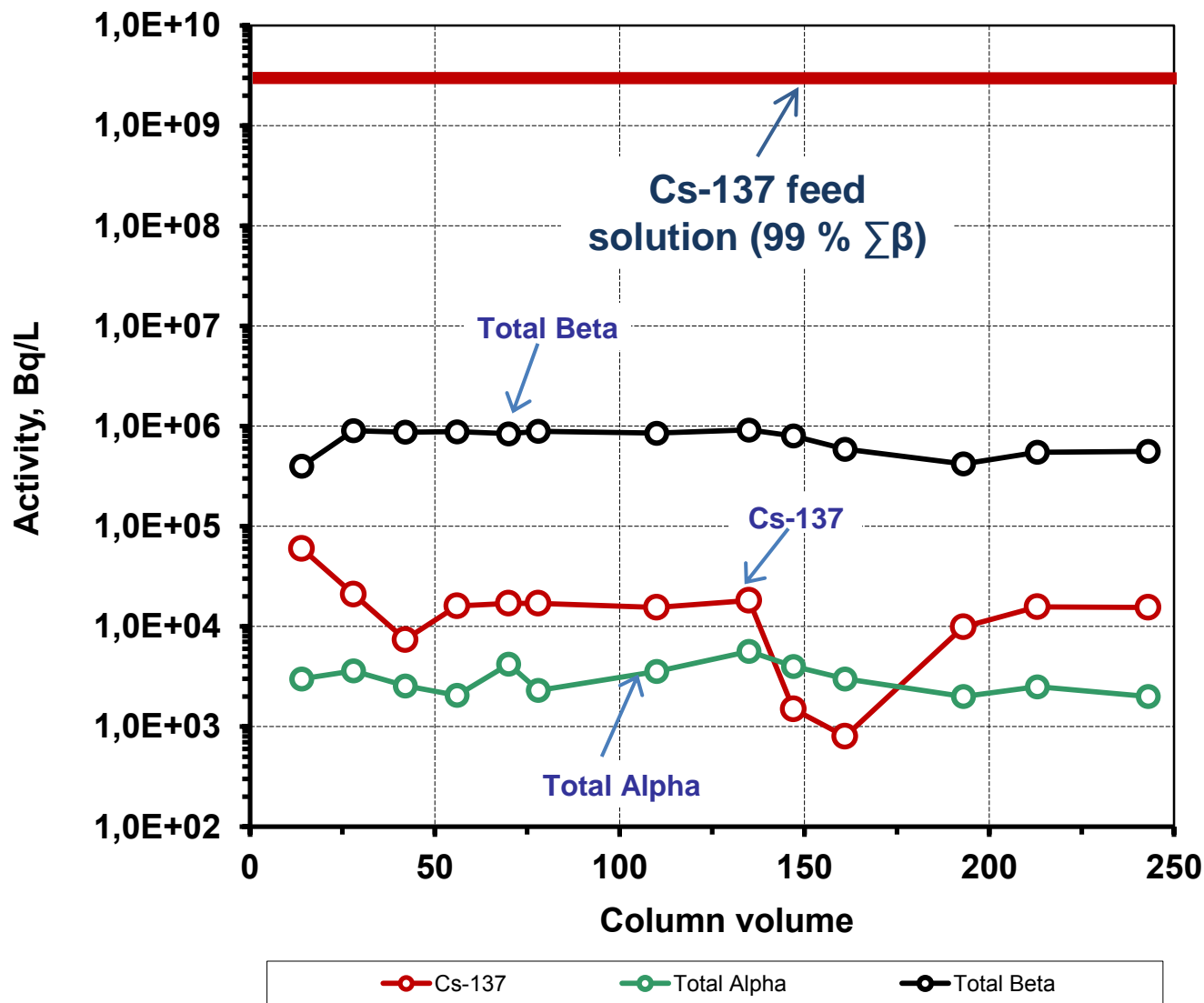




CLEVASOL dynamic sorption test with HLW solution (test 2)



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Feed solution

$4.1 \cdot 10^9$ Bq/L ^{137}Cs

$5.7 \cdot 10^7$ Bq/L ^{134}Cs

pH ~ 13.3

Averaged test results:

Filtrate activity

~ $1.8 \cdot 10^4$ Bq/L ^{137}Cs ,
DF = 300,000 (99,999%)

< 900 Bq/L ^{134}Cs ,
DF ~ 150,000 (99,999 %)

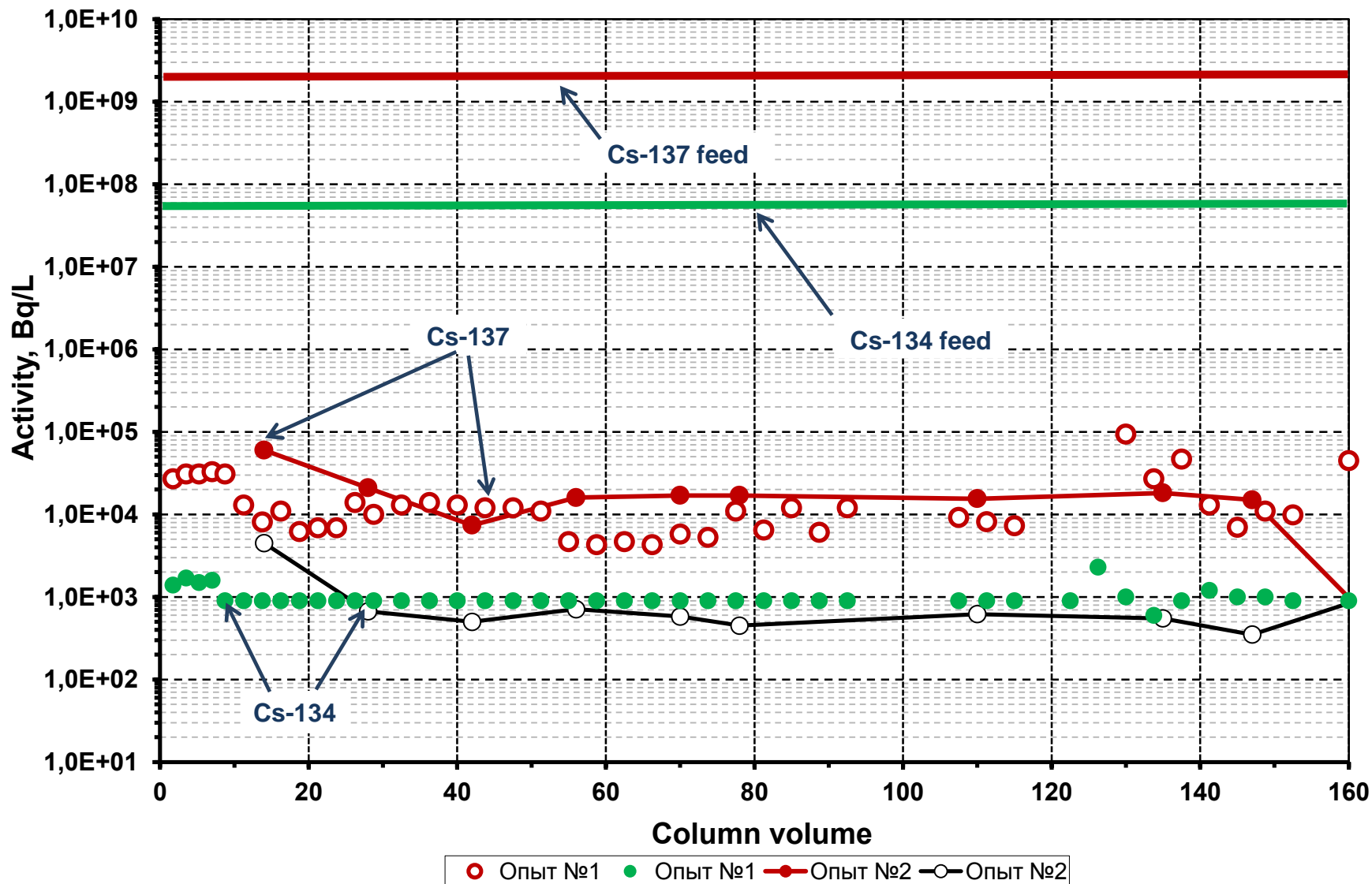




Comparison of HLW solution purification degree resulting from tests 1 and 2



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Testing results summary



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Static tests	Dynamic tests	
	pH 10	pH13
Solid/liquid = 1/10	Filter cycle 160 column volumes	Filter cycle 240 column volumes
Cs-137 DF ~ 20	Cs-137 DF ~ 23,000	Cs-137 DF ~ 300,000
Contact period: one day	Filtration rate ~ 1 to 5 column volumes	Filtration rate ~ 1 to 5 column volumes
Average activity $2.0 \cdot 10^8$ Bq/L	Average activity of the filtrate $7.4 \cdot 10^4$ Bq/L	Average activity of the filtrate $1.9 \cdot 10^4$ Bq/L
$K_d = 200$	Sorbent activity $2.5 \cdot 10^8$ Bq/g (6.8 Ci/kg)	Sorbent activity $4.0 \cdot 10^8$ Bq/g (10.8 Ci/kg)

Dynamic examinations of the CLEVASOL sorbent in test 1 were terminated because of the radiation safety requirements (MED 600 μ R/s). Sorbent capacity was not completely exhausted. Dynamic examinations of the CLEVASOL sorbent in test 2 are in progress.

Dynamic tests of the CLEVASOL sorbent demonstrated decontamination factors (DF) up to 10^6 in terms of Cs-137.





Future sorbent application



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Design flowsheet

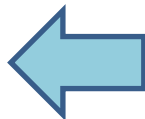
Liquid radwaste



Neutralization



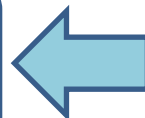
Filtration



Sludge handling



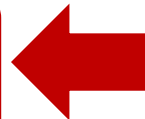
Solidification in cement



Cs sorption



Cs vitrification



Liquid radwaste



Filtration



Dilution



Cs sorption



Solidification in cement

Prospective flowsheet





Preliminary results of CLEVASOL sorbent tests can be considered as quite successful. Study of CLEVASOL sorbent are to be continued to specify its features and conditions (limits) of its applicability:

- effect of interfering cations (K, NH₄),
- radiation stability,
- chemical durability,
- regeneration efficiency, number of sorption/desorption cycles,
- spent sorbent management methods.

Successful implementation of the above mentioned tasks will allow large-scale reprocessing of legacy HLW.



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Thank you for your consideration!

